

Octane

Other names:	Oktan Oktanen Ottani UN 1262 n-C8H18 n-Octane
Inchi:	InChI=1S/C8H18/c1-3-5-7-8-6-4-2/h3-8H2,1-2H3
InchiKey:	TVMXDCGIABBOFY-UHFFFAOYSA-N
Formula:	C8H18
SMILES:	CCCCCCCC
Mol. weight [g/mol]:	114.23
CAS:	111-65-9

Physical Properties

Property code	Value	Unit	Source
af	0.3980		KDB
aigt	493.15	K	KDB
ap	343.750	K	KDB
chl	-5470.30 ± 1.60	kJ/mol	NIST Webbook
chl	-5270.40	kJ/mol	NIST Webbook
chl	-5441.30	kJ/mol	NIST Webbook
chl	-5471.80 ± 5.40	kJ/mol	NIST Webbook
chl	-5466.60	kJ/mol	NIST Webbook
chl	-5470.71 ± 0.67	kJ/mol	NIST Webbook
dm	0.00	debye	KDB
dvisc	0.0005180	Paxs	Thermophysical Properties of Binary Mixtures of 2-Methyl-1-propanol with Hexane, Octane, and Decane at 298.15 K
dvisc	0.0005180	Paxs	Study of densities, viscosities, and speeds of sound of binary liquid mixtures of butan-1-ol with n-alkanes (C6, C8, and C10) at T = (298.15, 303.15, and 308.15) K

dvisc	0.0005180	Paxs	Study of molecular interactions in binary liquid mixtures of 1-octanol with n-hexane, n-octane, and n-decane using volumetric, viscometric, and acoustic properties
fil	1.00	% in Air	KDB
flu	6.50	% in Air	KDB
fpo	286.48	K	KDB
gf	16.40	kJ/mol	KDB
gyrad	4.6800		KDB
hcg	5470.71	kJ/mol	KDB
hcn	5074.565	kJ/mol	KDB
hf	-208.40 ± 0.67	kJ/mol	NIST Webbook
hf	-208.60	kJ/mol	KDB
hf	-208.70	kJ/mol	NIST Webbook
hfl	-250.30 ± 1.80	kJ/mol	NIST Webbook
hfl	-250.00 ± 0.84	kJ/mol	NIST Webbook
hfus	16.48	kJ/mol	Joback Method
hvap	41.48	kJ/mol	NIST Webbook
hvap	41.60 ± 0.08	kJ/mol	NIST Webbook
hvap	41.60 ± 0.08	kJ/mol	NIST Webbook
hvap	34.00	kJ/mol	NIST Webbook
hvap	41.50	kJ/mol	NIST Webbook
hvap	41.50 ± 0.10	kJ/mol	NIST Webbook
hvap	41.53	kJ/mol	NIST Webbook
hvap	41.50 ± 0.10	kJ/mol	NIST Webbook
hvap	41.50 ± 0.10	kJ/mol	NIST Webbook
hvap	41.60	kJ/mol	NIST Webbook
ie	10.25	eV	NIST Webbook
ie	9.71 ± 0.15	eV	NIST Webbook
ie	9.80 ± 0.15	eV	NIST Webbook
ie	9.79	eV	NIST Webbook
ie	9.80 ± 0.10	eV	NIST Webbook
ie	10.01	eV	NIST Webbook
log10ws	-5.24		Aqueous Solubility Prediction Method
log10ws	-5.24		Estimated Solubility Method
logp	3.367		Crippen Method
mcvol	123.580	ml/mol	McGowan Method
nfpaf	%!d(float64=3)		KDB
pc	2487.00	kPa	NIST Webbook
pc	2486.93 ± 17.23	kPa	NIST Webbook
pc	2490.00	kPa	KDB
pc	2490.00 ± 30.00	kPa	NIST Webbook

pc	2495.00 ± 20.00	kPa	NIST Webbook
pc	2470.00 ± 98.07	kPa	NIST Webbook
pc	2480.00 ± 5.00	kPa	NIST Webbook
pc	2490.00 ± 30.00	kPa	NIST Webbook
pc	2497.12 ± 19.99	kPa	NIST Webbook
pc	2486.20 ± 40.53	kPa	NIST Webbook
pc	2488.00 ± 40.53	kPa	NIST Webbook
pc	2492.59 ± 50.66	kPa	NIST Webbook
pc	2497.10 ± 20.00	kPa	NIST Webbook
sg	467.06 ± 0.92	J/mol×K	NIST Webbook
sl	359.80	J/mol×K	NIST Webbook
sl	361.20	J/mol×K	NIST Webbook
sl	359.80	J/mol×K	NIST Webbook
tb	399.00 ± 0.60	K	NIST Webbook
tb	398.15 ± 1.00	K	NIST Webbook
tb	397.65 ± 0.30	K	NIST Webbook
tb	399.00 ± 0.70	K	NIST Webbook
tb	399.00 ± 1.00	K	NIST Webbook
tb	398.83	K	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
tb	398.95 ± 0.20	K	NIST Webbook
tb	397.75 ± 0.50	K	NIST Webbook
tb	398.74 ± 0.15	K	NIST Webbook
tb	398.55 ± 0.50	K	NIST Webbook
tb	398.35 ± 0.30	K	NIST Webbook
tb	398.74 ± 0.10	K	NIST Webbook
tb	398.75 ± 0.50	K	NIST Webbook
tb	398.55 ± 0.50	K	NIST Webbook
tb	396.00 ± 2.00	K	NIST Webbook
tb	398.15 ± 1.00	K	NIST Webbook
tb	398.95 ± 0.30	K	NIST Webbook
tb	398.15 ± 2.00	K	NIST Webbook
tb	398.95 ± 0.30	K	NIST Webbook
tb	398.64 ± 0.10	K	NIST Webbook
tb	398.45 ± 0.50	K	NIST Webbook
tb	398.82	K	KDB
tb	398.57	K	Isobaric vapor-liquid equilibrium for binary system of 2-ethylthiophene + n-octane at 101.33 kPa

tb	398.83	K	Solutions of alkyl methanoates and alkanes: Simultaneous modeling of phase equilibria and mixing properties. Estimation of behavior by UNIFAC with recalculation of parameters
tb	398.79	K	Isothermal and isobaric (vapour + liquid) equilibria of (alpha-pinene + n-butanol + n-octane)
tb	398.60	K	Excess molar volumes of the ternary system {methylcyclohexane (1) + cyclohexane (2) + n-alkanes (3)} at T = 298.15 K
tb	399.15	K	Excess volumes, densities, speeds of sound and viscosities for the binary systems of diisopropyl ether with hydrocarbons at 303.15K
tb	398.65	K	Densities and Excess Molar Properties of Dimethyl Carbonate with Alkanes (C6 to C10) and VLE of Dimethyl Carbonate with Alkanes (C9 to C10) at 101.3 kPa
tb	396.70 ± 1.50	K	NIST Webbook
tb	398.49	K	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
tb	398.74	K	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
tb	398.80 ± 0.20	K	NIST Webbook
tb	398.80 ± 0.20	K	NIST Webbook
tb	398.90	K	NIST Webbook
tb	398.73 ± 0.10	K	NIST Webbook
tb	398.80	K	NIST Webbook
tb	398.76 ± 0.20	K	NIST Webbook
tb	398.96 ± 0.20	K	NIST Webbook
tb	398.96 ± 0.50	K	NIST Webbook
tb	398.93 ± 0.08	K	NIST Webbook
tb	398.70 ± 0.50	K	NIST Webbook
tb	398.75 ± 0.15	K	NIST Webbook
tb	398.55 ± 0.20	K	NIST Webbook
tb	398.12 ± 0.20	K	NIST Webbook
tb	398.77 ± 0.10	K	NIST Webbook

tb	398.95 ± 0.40	K	NIST Webbook
tb	398.76 ± 0.20	K	NIST Webbook
tb	398.75 ± 0.50	K	NIST Webbook
tb	398.55 ± 0.30	K	NIST Webbook
tb	398.77 ± 0.15	K	NIST Webbook
tb	398.27 ± 0.30	K	NIST Webbook
tb	398.15 ± 0.60	K	NIST Webbook
tb	398.40 ± 1.00	K	NIST Webbook
tb	398.85 ± 0.25	K	NIST Webbook
tb	398.82 ± 0.30	K	NIST Webbook
tb	399.15 ± 1.50	K	NIST Webbook
tb	397.80 ± 0.30	K	NIST Webbook
tb	396.40 ± 2.00	K	NIST Webbook
tb	398.85 ± 0.40	K	NIST Webbook
tb	399.09 ± 0.30	K	NIST Webbook
tb	398.75 ± 0.10	K	NIST Webbook
tb	398.81 ± 0.44	K	NIST Webbook
tb	398.55 ± 0.30	K	NIST Webbook
tb	398.71 ± 0.20	K	NIST Webbook
tb	398.80 ± 0.40	K	NIST Webbook
tb	398.95 ± 0.50	K	NIST Webbook
tb	393.15 ± 3.00	K	NIST Webbook
tb	398.81 ± 0.10	K	NIST Webbook
tb	398.90 ± 0.20	K	NIST Webbook
tb	398.25 ± 0.30	K	NIST Webbook
tb	398.62 ± 0.30	K	NIST Webbook
tb	397.85 ± 0.30	K	NIST Webbook
tb	397.20 ± 2.00	K	NIST Webbook
tb	398.75 ± 0.30	K	NIST Webbook
tb	398.55 ± 0.50	K	NIST Webbook
tb	398.85 ± 0.50	K	NIST Webbook
tb	397.35 ± 0.50	K	NIST Webbook
tb	398.75 ± 0.30	K	NIST Webbook
tb	398.90 ± 0.30	K	NIST Webbook
tb	398.75 ± 0.40	K	NIST Webbook
tb	398.81 ± 0.01	K	NIST Webbook
tb	397.65 ± 0.50	K	NIST Webbook
tb	397.40 ± 1.00	K	NIST Webbook
tb	398.15 ± 2.00	K	NIST Webbook
tb	398.70 ± 0.20	K	NIST Webbook
tb	398.95 ± 0.50	K	NIST Webbook
tb	398.90 ± 0.20	K	NIST Webbook
tb	398.75 ± 0.30	K	NIST Webbook
tb	398.81 ± 0.10	K	NIST Webbook

tb	398.80 ± 0.30	K	NIST Webbook
tb	397.15 ± 1.00	K	NIST Webbook
tb	398.75 ± 0.20	K	NIST Webbook
tb	401.65 ± 0.50	K	NIST Webbook
tb	398.75 ± 0.30	K	NIST Webbook
tb	398.90 ± 0.20	K	NIST Webbook
tb	398.81 ± 0.20	K	NIST Webbook
tb	398.95 ± 0.20	K	NIST Webbook
tb	398.80 ± 0.05	K	NIST Webbook
tb	398.80 ± 0.40	K	NIST Webbook
tc	568.92	K	Determination of the Critical Properties of C6 C10 n-Alkanes and Their Binary Systems Using a Flow Apparatus
tc	568.80	K	The Critical Temperatures of a Number of (i) (Chloroalkane (C3 C4) + Hydrocarbon (C6 C7)) Binary Mixtures and (ii) (Aromatic Halocarbon (Chlorobenzene, Fluorobenzene, 1,2-Dichlorobenzene, or 1,3-Dichlorobenzene) + Alkane (C8)) Binary Mixtures
tc	568.90	K	Measurement of Critical Properties for Binary and Ternary Mixtures Containing n-Butanol and n-Alkane
tc	568.92	K	Experimental determination of critical data of multi-component mixtures containing potential gasoline additives 2-butanol by a flow-type apparatus
tc	568.90	K	Measurement of critical properties for binary and ternary mixtures containing potential gasoline additive diethyl carbonate (DEC)
tc	568.70	K	KDB
tf	216.26	K	Aqueous Solubility Prediction Method
tf	216.30	K	KDB
tt	216.37	K	KDB
tt	216.37 ± 0.40	K	NIST Webbook
tt	216.37 ± 0.03	K	NIST Webbook
tt	216.36 ± 0.20	K	NIST Webbook
tt	216.37 ± 0.20	K	NIST Webbook
tt	216.36 ± 0.05	K	NIST Webbook

tt	216.37 ± 0.02	K	NIST Webbook
tt	215.80 ± 0.20	K	NIST Webbook
tt	215.85 ± 0.20	K	NIST Webbook
tt	215.60 ± 0.25	K	NIST Webbook
vc	0.492	m ³ /kmol	KDB
vc	0.492	m ³ /kmol	NIST Webbook
zc	0.2590860		KDB
zra	0.26		KDB

Temperature Dependent Properties

Property code	Value	Unit	Temperature [K]	Source
cpg	238.95 ± 0.48	J/mol×K	398.15	NIST Webbook
cpg	242.67	J/mol×K	405.70	NIST Webbook
cpg	250.59 ± 0.50	J/mol×K	423.15	NIST Webbook
cpg	263.02 ± 0.53	J/mol×K	448.15	NIST Webbook
cpg	297.00 ± 0.59	J/mol×K	523.15	NIST Webbook
cpg	274.84 ± 0.55	J/mol×K	473.15	NIST Webbook
cpg	285.98 ± 0.57	J/mol×K	498.15	NIST Webbook
cpg	295.39	J/mol×K	522.70	NIST Webbook
cpg	270.70	J/mol×K	462.50	NIST Webbook
cpg	232.74 ± 0.47	J/mol×K	385.65	NIST Webbook
cpl	253.94	J/mol×K	298.15	Thermodynamic behaviour of the binary systems dimethyl carbonate + n-octane or n-nonane
cpl	254.14	J/mol×K	298.15	NIST Webbook
cpl	253.20	J/mol×K	298.00	NIST Webbook
cpl	252.92	J/mol×K	298.15	NIST Webbook
cpl	254.07	J/mol×K	298.15	NIST Webbook
cpl	252.40	J/mol×K	298.00	NIST Webbook
cpl	254.02	J/mol×K	298.15	NIST Webbook
cpl	252.40	J/mol×K	297.54	NIST Webbook
cpl	253.72	J/mol×K	298.15	NIST Webbook
cpl	254.18	J/mol×K	298.15	NIST Webbook
cpl	255.68	J/mol×K	298.15	NIST Webbook
cpl	254.11	J/mol×K	298.15	NIST Webbook
cpl	255.68	J/mol×K	298.15	NIST Webbook
cpl	255.68	J/mol×K	298.15	NIST Webbook
cpl	255.68	J/mol×K	298.15	NIST Webbook

cpl	262.20	J/mol×K	318.15	NIST Webbook
cpl	254.70	J/mol×K	299.00	NIST Webbook
cpl	269.31	J/mol×K	333.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	267.24	J/mol×K	328.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	264.78	J/mol×K	323.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	262.70	J/mol×K	318.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	260.87	J/mol×K	313.16	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions

cpl	258.05	J/mol×K	308.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	253.89	J/mol×K	298.15	NIST Webbook
cpl	256.50	J/mol×K	303.16	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	253.98	J/mol×K	298.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	252.24	J/mol×K	293.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	250.10	J/mol×K	288.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
cpl	253.93	J/mol×K	299.80	NIST Webbook

cpl	258.03	J/mol×K	308.15	Thermodynamic behaviour of the binary systems dimethyl carbonate + n-octane or n-nonane
cpl	251.50	J/mol×K	298.30	NIST Webbook
cpl	250.12	J/mol×K	288.15	Thermodynamic behaviour of the binary systems dimethyl carbonate + n-octane or n-nonane
cpl	247.70	J/mol×K	293.70	NIST Webbook
cpl	248.16	J/mol×K	283.15	Excess Molar Enthalpies and Heat Capacities of {2-Methylpiperidine Water} and {N-Methylpiperidine Water} Systems of Low to Moderate Amine Compositions
dvisc	0.0004720	Paxs	303.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0004500	Paxs	308.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K

dvisc	0.0004910	Paxs	303.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K
dvisc	0.0005087	Paxs	298.15	Viscosity and Density of Binary Mixtures of Ethyl Alcohol with n-Alkanes (C6, C8, and C10)
dvisc	0.0005374	Paxs	293.15	Viscosity and Density of Binary Mixtures of Ethyl Alcohol with n-Alkanes (C6, C8, and C10)
dvisc	0.0004358	Paxs	313.15	Densities and Viscosities of Binary Mixtures of JP-10 with n-Octane or n-Decane at Several Temperatures
dvisc	0.0004795	Paxs	303.15	Densities and Viscosities of Binary Mixtures of JP-10 with n-Octane or n-Decane at Several Temperatures
dvisc	0.0005177	Paxs	298.15	Densities and Viscosities of Binary Mixtures of JP-10 with n-Octane or n-Decane at Several Temperatures
dvisc	0.0005439	Paxs	293.15	Densities and Viscosities of Binary Mixtures of JP-10 with n-Octane or n-Decane at Several Temperatures

dvisc	0.0003570	Paxs	333.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0003750	Paxs	328.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0004426	Paxs	313.30	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0003940	Paxs	323.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0004150	Paxs	318.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0004340	Paxs	313.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0004590	Paxs	308.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0004860	Paxs	303.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K

dvisc	0.0005140	Paxs	298.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0005450	Paxs	293.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0005840	Paxs	288.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0006230	Paxs	283.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0006710	Paxs	278.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0007180	Paxs	273.15	Densities and Viscosities of MTBE + Heptane or Octane at p) 0.1 MPa from (273.15 to 363.15) K
dvisc	0.0002840	Paxs	353.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003139	Paxs	343.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures

dvisc	0.0003495	Paxs	333.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0003864	Paxs	323.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0004306	Paxs	313.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0004837	Paxs	303.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0005206	Paxs	298.15	Thermodynamic Properties of Binary Mixtures of p-Xylene with Cyclohexane, Heptane, Octane, and N-Methyl-2-pyrrolidone at Several Temperatures
dvisc	0.0002610	Paxs	363.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure

dvisc	0.0002870	Paxs	353.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0003140	Paxs	343.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0003430	Paxs	333.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0003800	Paxs	323.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0004220	Paxs	313.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure

dvisc	0.0004150	Paxs	313.15	Density, Viscosity, and Speed of Sound of (Methyl Benzoate + Cyclohexane), (Methyl Benzoate + n-Hexane), (Methyl Benzoate + Heptane), and (Methyl Benzoate + Octane) at Temperatures of (303.15, 308.15, and 313.15) K
dvisc	0.0005010	Paxs	298.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0004300	Paxs	313.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.
dvisc	0.0004780	Paxs	303.15	Dynamic Viscosities of 2-Pentanol with Alkanes (Octane, Decane, and Dodecane) at Three Temperatures T) (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO Interaction Parameters

dvisc	0.0005060	Paxs	298.15	Dynamic Viscosities of 2-Pentanol with Alkanes (Octane, Decane, and Dodecane) at Three Temperatures T) (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO Interaction Parameters
dvisc	0.0005380	Paxs	293.15	Dynamic viscosities of 2-butanol with alkanes (C8, C10, and C12) at several temperatures
dvisc	0.0005060	Paxs	298.15	Dynamic viscosities of 2-butanol with alkanes (C8, C10, and C12) at several temperatures
dvisc	0.0004780	Paxs	303.15	Dynamic viscosities of 2-butanol with alkanes (C8, C10, and C12) at several temperatures
dvisc	0.0004911	Paxs	303.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0004414	Paxs	313.30	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer

dvisc	0.0003967	Paxs	323.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0003632	Paxs	333.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0003352	Paxs	343.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0003012	Paxs	353.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0002766	Paxs	363.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0002545	Paxs	373.30	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer

dvisc	0.0002341	Paxs	383.00	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0002208	Paxs	393.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0002021	Paxs	403.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001924	Paxs	413.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001762	Paxs	423.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001642	Paxs	433.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer

dvisc	0.0001527	Paxs	443.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001416	Paxs	453.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001322	Paxs	463.20	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001228	Paxs	473.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001139	Paxs	483.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0001069	Paxs	493.10	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer

dvisc	0.0000995	Paxs	503.00	Viscosity measurements of hydrocarbon fuel at temperatures from (303.2 to 513.2) K and pressures up to 5.1 MPa using a two-capillary viscometer
dvisc	0.0004913	Paxs	303.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0005380	Paxs	293.15	Dynamic Viscosities of 2-Pentanol with Alkanes (Octane, Decane, and Dodecane) at Three Temperatures T) (293.15, 298.15, and 303.15) K. New UNIFAC-VISCO Interaction Parameters
dvisc	0.0003961	Paxs	323.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0003634	Paxs	333.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0003311	Paxs	343.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa

dvisc	0.0003013	Paxs	353.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0002765	Paxs	363.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0002540	Paxs	373.30	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0002340	Paxs	383.00	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0002205	Paxs	393.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0002019	Paxs	403.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001905	Paxs	413.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa

dvisc	0.0001761	Paxs	423.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001643	Paxs	433.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001526	Paxs	443.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001417	Paxs	453.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001321	Paxs	463.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001228	Paxs	473.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0001138	Paxs	483.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa

dvisc	0.0001068	Paxs	493.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000993	Paxs	503.00	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000901	Paxs	513.20	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000825	Paxs	523.30	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000753	Paxs	533.40	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000678	Paxs	543.40	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000607	Paxs	553.40	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa

dvisc	0.0005340	Paxs	293.15	Densities and Viscosities of Binary Mixtures of Ethylbenzene + N-Methyl-2-pyrrolidone, Ethylbenzene + Sulfolane, and Styrene + Octane from (303.15 to 353.15) K and Atmospheric Pressure
dvisc	0.0000444	Paxs	573.30	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0000325	Paxs	583.10	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
dvisc	0.0005014	Paxs	303.20	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa
dvisc	0.0003078	Paxs	353.10	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa
dvisc	0.0002070	Paxs	403.20	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa
dvisc	0.0001465	Paxs	453.10	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa
dvisc	0.0001049	Paxs	503.00	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa

dvisc	0.0000692	Paxs	553.40	Experimental Measurement of JP-10 Viscosity at 242.7-753.3 K under Pressures up to 6.00 MPa
dvisc	0.0006247	Paxs	283.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0005523	Paxs	293.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0004828	Paxs	303.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0004320	Paxs	313.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0003870	Paxs	323.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering

dvisc	0.0003079	Paxs	348.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0002487	Paxs	373.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0002028	Paxs	398.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0001665	Paxs	423.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0001393	Paxs	448.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0001168	Paxs	473.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering

dvisc	0.0000947	Paxs	498.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0000755	Paxs	523.15	Liquid Viscosity and Surface Tension of n-Hexane, n-Octane, n-Decane, and n-Hexadecane up to 573 K by Surface Light Scattering
dvisc	0.0006140	Paxs	283.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.
dvisc	0.0005420	Paxs	293.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.

dvisc	0.0005080	Paxs	298.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.
dvisc	0.0004830	Paxs	303.15	A Study on Properties Derived from Densities and Viscosities for the Ternary Systems (Methyl Pentanoate or Methyl Heptanoate) + n-Octane + 1-Hexanol and their Binary Subsystems at Various Temperatures.
dvisc	0.0000532	Paxs	563.30	Viscosity Measurement of Endothermic Fuels at Temperatures from 303 K to 673 K and Pressures up to 5.00 MPa
hfust	20.09	kJ/mol	215.60	NIST Webbook
hfust	20.65	kJ/mol	215.80	NIST Webbook
hfust	20.74	kJ/mol	216.40	NIST Webbook
hfust	21.80	kJ/mol	216.60	NIST Webbook
hfust	20.74	kJ/mol	216.38	NIST Webbook
hsubt	68.10	kJ/mol	216.00	NIST Webbook
hvapt	39.10 ± 0.10	kJ/mol	333.00	NIST Webbook
hvapt	35.40 ± 0.10	kJ/mol	344.00	NIST Webbook
hvapt	36.70 ± 0.10	kJ/mol	328.00	NIST Webbook
hvapt	38.00 ± 0.10	kJ/mol	311.00	NIST Webbook
hvapt	43.00	kJ/mol	257.00	NIST Webbook
hvapt	37.80 ± 0.10	kJ/mol	353.00	NIST Webbook
hvapt	39.20	kJ/mol	363.00	NIST Webbook
hvapt	40.50 ± 0.10	kJ/mol	313.00	NIST Webbook
hvapt	41.90	kJ/mol	315.50	NIST Webbook
hvapt	41.20	kJ/mol	348.50	NIST Webbook

hvapt	34.90	kJ/mol	537.50	NIST Webbook
hvapt	35.50	kJ/mol	469.00	NIST Webbook
hvapt	36.30	kJ/mol	414.00	NIST Webbook
hvapt	44.40	kJ/mol	247.00	NIST Webbook
hvapt	39.40	kJ/mol	443.00	NIST Webbook
hvapt	34.41	kJ/mol	398.80	NIST Webbook
hvapt	41.75	kJ/mol	298.00	Enthalpies of Vaporization and Vapor Pressures of Some Deuterated Hydrocarbons. Liquid-Vapor Pressure Isotope Effects
hvapt	34.41	kJ/mol	398.80	KDB
hvapt	41.00	kJ/mol	348.50	NIST Webbook
pvap	60.63	kPa	381.34	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	121.60	kPa	405.51	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	119.25	kPa	404.79	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	117.10	kPa	404.10	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	116.17	kPa	403.81	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	113.09	kPa	402.81	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	110.71	kPa	402.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	108.30	kPa	401.23	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	106.23	kPa	400.53	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	103.61	kPa	399.61	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	101.32	kPa	398.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	100.68	kPa	398.59	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	99.59	kPa	398.19	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	98.73	kPa	397.90	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	96.14	kPa	396.95	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	93.64	kPa	396.04	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	124.10	kPa	406.27	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	91.38	kPa	395.14	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	89.39	kPa	394.37	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	87.09	kPa	393.47	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	84.94	kPa	392.60	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	82.51	kPa	391.60	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	80.05	kPa	390.56	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	77.94	kPa	389.65	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	75.43	kPa	388.55	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	73.02	kPa	387.45	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	70.52	kPa	386.29	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	65.07	kPa	383.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	62.68	kPa	382.42	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	126.61	kPa	407.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	58.20	kPa	380.03	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	55.02	kPa	378.25	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	52.90	kPa	377.00	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	50.59	kPa	375.61	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	48.04	kPa	374.01	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	45.57	kPa	372.39	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	43.19	kPa	370.77	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	40.82	kPa	369.09	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	38.88	kPa	367.65	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	36.53	kPa	365.82	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	34.16	kPa	363.86	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	31.58	kPa	361.59	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	28.55	kPa	358.82	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	26.70	kPa	356.97	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	25.56	kPa	355.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	23.14	kPa	353.05	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	21.09	kPa	350.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	60.00	kPa	380.84	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	380.78	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	380.87	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	380.76	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	380.85	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	60.00	kPa	380.94	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	129.50	kPa	407.89	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	132.46	kPa	408.75	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	135.53	kPa	409.62	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	137.42	kPa	410.15	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	67.34	kPa	384.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	139.87	kPa	410.83	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	185.56	kPa	422.10	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	188.02	kPa	422.64	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	190.85	kPa	423.26	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	193.15	kPa	423.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	195.02	kPa	424.15	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	197.87	kPa	424.76	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
pvap	199.97	kPa	425.20	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)

pvap	30.00	kPa	359.76	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	60.00	kPa	380.43	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	90.00	kPa	394.09	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	101.30	kPa	398.49	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	30.00	kPa	360.06	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	60.00	kPa	380.94	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	90.00	kPa	394.60	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System
pvap	101.30	kPa	398.74	Measurement and Modeling of Vapor Liquid Equilibria for the Octane + Sulfuric Acid + Water + Ethanol System

pvap	40.00	kPa	368.32	Vapor Liquid Equilibria Measurements for the Nine n-Alkane/Ketone Pairs Comprising 2-, 3-, and 4-Heptanone with n-Octane, n-Nonane, and n-Decane
pvap	40.00	kPa	367.97	Vapor Liquid Equilibria Measurements for the Nine n-Alkane/Ketone Pairs Comprising 2-, 3-, and 4-Heptanone with n-Octane, n-Nonane, and n-Decane
pvap	40.00	kPa	368.30	Vapor Liquid Equilibria Measurements for the Nine n-Alkane/Ketone Pairs Comprising 2-, 3-, and 4-Heptanone with n-Octane, n-Nonane, and n-Decane
pvap	60.00	kPa	380.82	Vapor Liquid Equilibria Measurements for the Five Linear C6 Esters with n-Octane
pvap	101.33	kPa	398.57	Isobaric vapor-liquid equilibrium for binary system of 2-ethylthiophene + n-octane at 101.33 kPa
pvap	23.16	kPa	353.15	Measurement of vapor-liquid equilibria (VLE) and excess enthalpies (HE) of binary systems with 1-alkyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide and prediction of these properties and A using modified UNIFAC (Dortmund)

pvap	33.91	kPa	363.15	An equipment for dynamic measurements of vapour liquid equilibria and results in binary systems containing cyclohexylamine
pvap	23.61	kPa	353.15	An equipment for dynamic measurements of vapour liquid equilibria and results in binary systems containing cyclohexylamine
pvap	16.04	kPa	343.15	An equipment for dynamic measurements of vapour liquid equilibria and results in binary systems containing cyclohexylamine
pvap	10.59	kPa	333.15	An equipment for dynamic measurements of vapour liquid equilibria and results in binary systems containing cyclohexylamine
pvap	114.65	kPa	403.32	Measurements of the Excess Properties and Vapor-Liquid Equilibria at 101.32 kPa for Mixtures of Ethyl Ethanoate + Alkanes (from C5 to C10)
rfi	1.39540		298.15	Solubilities of Bis (2,2,6,6-Tetramethyl-4-Piperidiny) Maleate in Hexane, Heptane, Octane, m-Xylene and Tetrahydrofuran from (253.15 to 310.15) K

rfi	1.39780	298.10	Excess Enthalpies and Thermal Conductivity Coefficients for Binary Mixtures of Carbon Tetrachloride and Four Alkanes (C5 to C8) at a Temperature of 298.15 K
rfi	1.39650	293.15	Isobaric Vapor-Liquid Equilibria of Hexane + 1-Decene and Octane + 1-Decene Mixtures
rfi	1.38550	318.15	Multiproperty Correlation of Experimental Data of the Binaries Propyl Ethanoate + Alkanes (Pentane to Decane). New Experimental Information for Vapor Liquid Equilibrium and Mixing Properties
rfi	1.39520	298.15	Multiproperty Correlation of Experimental Data of the Binaries Propyl Ethanoate + Alkanes (Pentane to Decane). New Experimental Information for Vapor Liquid Equilibrium and Mixing Properties
rfi	1.39230	303.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of 1,2,3,4-Tetrahydronaphthalene with Some n-Alkanes at T = (293.15 to 313.15) K

rfi	1.39700	293.15	Densities, Viscosities, and Refractive Indices of Binary Mixtures of 1,2,3,4-Tetrahydronaphthalene with Some n-Alkanes at T = (293.15 to 313.15) K
rfi	1.39519	298.15	Extraction of Benzene from Aliphatic Compounds Using Commercial Ionic Liquids as Solvents: Study of the Liquid-Liquid Equilibrium at T = 298.15 K
rfi	1.39519	298.15	Liquid-Liquid Equilibria of the Ternary Systems of Alkane + Aromatic + 1-Ethylpyridinium Ethylsulfate Ionic Liquid at T = (283.15 and 298.15) K
rfi	1.39519	298.15	Separation of Benzene from Linear Alkanes (C6-C9) Using 1-Ethyl-3-Methylimidazolium Ethylsulfate at T = 298.15 K
rfi	1.39460	298.15	Ternary Liquid-Liquid(-Liquid) Equilibria of Aniline + Cyclohexylamine + Water, Aniline + Cyclohexylamine + Octane, Aniline + Water + Toluene, and Aniline + Water + Octane

rfi	1.39460	298.15	Liquid-Liquid(-Liquid) Equilibria in Ternary Systems of Water + Cyclohexylamine + Aromatic Hydrocarbon (Toluene or Propylbenzene) or Aliphatic Hydrocarbon (Heptane or Octane)
rfi	1.39730	293.15	Vapor-Liquid Equilibria for the Binary Mixture alpha-Pinene + Octane
rfi	1.39750	293.15	Infinite Dilution Activity Coefficients of Hydrocarbons in Triethylene Glycol and Tetraethylene Glycol
rfi	1.39550	298.15	Measurement and Prediction of Excess Properties of Binary Mixtures Methyl Decanoate + an Even-Numbered n-Alkane (C6-C16) at 298.15 K
rfi	1.39530	298.15	Isothermal Bubble Pressure Data for the Binary System of C2F6 and n-Octane
rfi	1.39780	293.15	Isothermal Bubble Pressure Data for the Binary System of C2F6 and n-Octane
rfi	1.39800	298.15	P-rho-T Data and Modeling for Propan-1-ol + n-Octane or n-Nonane or n-Decane from 313.15 K to 363.15 K and 1 MPa to 20 MPa

rfi	1.39510	298.15	Density, Surface Tension, and Refractive Index of Octane + 1-Alkanol Mixtures at T) 298.15 K.
rfi	1.39520	298.15	A Study on Alkane + Ester + Ester Systems. Physicochemical Behavior of Binaries and Ternaries of Octane or Iso-octane with Methyl Esters (Ethanoate, Butanoate, Pentanoate)
rfi	1.39780	293.15	Experimental solubility for betulin and estrone in various solvents within the temperature range T = (293.2 to 328.2) K
rfi	1.39519	298.15	Extraction of toluene from aliphatic compounds using an ionic liquid as solvent: Influence of the alkane on the (liquid + liquid) equilibrium
rfi	1.40070	284.73	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40120	283.88	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region

rfi	1.40170	282.65	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40210	281.66	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40270	280.51	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40280	280.36	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40320	279.68	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.40400	277.80	The measurements of coexistence curves and light scattering for $\{x\text{C}_6\text{H}_5\text{CN} + (1-x)\text{CH}_3(\text{CH}_2)_6\text{CH}_3\}$ in the critical region
rfi	1.39500	298.15	p, V _m , T) measurements of (octane + benzene) at temperatures from (298.15 to 328.15) K and at pressures up to 40 MPa

rfi	1.39500	298.15	Excess molar volumes of (octane + benzene, or toluene, or 1,3-xylene, or 1,3,5-trimethylbenzene) at temperatures between (298.15 and 328.15) K
rfi	1.39500	298.15	(P, V _m , T) Measurements of (octane + 1-chlorohexane) at temperatures from 298.15 K to 328.15 K and at pressures up to 40 MPa
rfi	1.38880	308.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.39160	303.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C6 to C12) at T = 298.15 K to T = 308.15 K
rfi	1.39260	303.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.39470	298.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.39650	293.15	Physical properties of {anisole + n-alkanes} at temperatures between (293.15 and 303.15) K
rfi	1.39538	298.15	Liquid liquid equilibria of lactam containing binary systems

rfi	1.39460	298.15	Vapor liquid equilibria in ternary systems of associating components (water, aniline, cyclohexylamine) and hydrocarbons (octane or toluene)
rfi	1.39504	298.15	Separation of aromatic hydrocarbons from alkanes using ammonium ionic liquid C ₂ N ₂ F ₂ at T = 298.15K
rfi	1.53910	298.15	(Vapor + liquid) equilibrium of binary mixtures formed by N,N-dimethyl formamide with some compounds at 95.1 kPa
rfi	1.39460	298.15	Activity Coefficients at Infinite Dilution of Cyclohexylamine + Octane, Toluene, Ethylbenzene, or Aniline and Excess Molar Volumes in Binary Mixtures of Cyclohexylamine + Heptane, Octane, Nonane, Decane, Undecane, Aniline, or Water
rfi	1.39505	298.15	KDB
rfi	1.39470	298.15	Excess properties of the binary mixtures of methylcyclohexane + alkanes (C ₆ to C ₁₂) at T = 298.15 K to T = 308.15 K
rfi	1.39730	293.15	Limiting Activity Coefficients by Comparative Tensimetry: 1-Propanol and 1-Butanol in Heptane and in Octane

rho	698.71	kg/m ³	298.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho	686.36	kg/m ³	313.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho	682.26	kg/m ³	318.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho	678.13	kg/m ³	323.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho	706.54	kg/m ³	288.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	702.53	kg/m ³	293.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa

rho	698.51	kg/m ³	298.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	694.48	kg/m ³	303.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	690.42	kg/m ³	308.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	686.34	kg/m ³	313.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	682.24	kg/m ³	318.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	690.44	kg/m ³	308.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho	673.95	kg/m ³	328.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho	669.77	kg/m ³	333.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa

rho1	665.55	kg/m3	338.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho1	661.28	kg/m3	343.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rho1	703.00	kg/m3	293.15	Experimental Solubility Data for Binary Mixtures of Ethane and 2,2,4-Trimethylpentane at Pressures up to 6 MPa Using a New Variable-Volume Sapphire Cell
rho1	698.71	kg/m3	298.15	Liquid-Liquid Equilibria for 2-Phenylethan-1-ol + Alkane Systems
rho1	698.70	kg/m3	298.15	Liquid-Liquid Equilibrium Data for Ternary Systems Containing Alkanes (n-Pentane, n-Hexane, n-Heptane, and n-Octane) + Alcohol (Methanol and Ethanol) + Protic Ionic Liquid (2-HEAF)
rho1	698.50	kg/m3	298.15	Viscosities of Dimethyl Carbonate or Diethyl Carbonate with Alkanes at Four Temperatures. New UNIFAC-VISCO Parameters

rhoI	702.87	kg/m ³	293.15	Excess Molar Enthalpies for Binary Mixtures of Ethanol + Acetone, + Octane, + Cyclohexane and 1-Propanol + Acetone, + Octane, + Heptane at 323.15
rhoI	698.72	kg/m ³	298.15	Excess Enthalpies of the Ternary Mixtures: Diisopropyl Ether + 3-Methylpentane + (Octane or Decane) at 298.15 K
rhoI	698.72	kg/m ³	298.15	Excess Enthalpies of Binary Mixtures of 1-Hexene with Some n-Alkanes at 298.15 K
rhoI	698.55	kg/m ³	298.15	Thermodynamics of Mixtures Containing Ethers. Part III. Liquid-Liquid Equilibria for 2,5,8,11-Tetraoxadodecane or 2,5,8,11,14-Pentaoxapentadecane + Selected N-Alkanes
rhoI	698.64	kg/m ³	298.15	Thermodynamics of Mixtures Containing a Strongly Polar Compound. 8. Liquid-Liquid Equilibria for N,N-Dialkylamide + Selected N-Alkanes
rhoI	710.76	kg/m ³	283.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rhoI	706.76	kg/m ³	288.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}

rho1	702.74	kg/m3	293.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho1	694.49	kg/m3	303.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho1	694.66	kg/m3	303.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho1	690.58	kg/m3	308.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho1	686.49	kg/m3	313.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho1	682.37	kg/m3	318.15	Measurements of Density and Heat Capacity for Binary Mixtures {x Benzonitrile + (1 -x) (Octane or Nonane)}
rho1	698.49	kg/m3	298.15	Liquid-Liquid(-Liquid) Equilibria in Ternary Systems of Aliphatic Hydrocarbons (Heptane or Octane) + Phenols + Water

rho	694.52	kg/m ³	303.15	Vapor-Liquid Equilibria in Ternary Systems of Toluene or Octane + Phenols + Water
rho	698.57	kg/m ³	298.20	Apparent and Partial Molar Volumes at Infinite Dilution and Solid Liquid Equilibria of Dibenzothiophene + Alkane Systems
rho	686.37	kg/m ³	313.20	Apparent and Partial Molar Volumes at Infinite Dilution and Solid Liquid Equilibria of Dibenzothiophene + Alkane Systems
rho	718.25	kg/m ³	273.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	698.53	kg/m ³	298.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho	710.34	kg/m ³	283.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa

rho	706.35	kg/m ³	288.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	702.35	kg/m ³	293.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	698.34	kg/m ³	298.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	694.30	kg/m ³	303.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	690.24	kg/m ³	308.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	686.17	kg/m ³	313.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa

rho	682.06	kg/m ³	318.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	677.94	kg/m ³	323.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	673.79	kg/m ³	328.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	669.61	kg/m ³	333.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	665.40	kg/m ³	338.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho	661.16	kg/m ³	343.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa

rho1	656.88	kg/m3	348.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho1	652.57	kg/m3	353.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho1	648.23	kg/m3	358.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho1	643.83	kg/m3	363.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rho1	698.76	kg/m3	298.15	Thermodynamics of Mixtures Containing Aromatic Alcohols. 1. Liquid Liquid Equilibria for (Phenylmethanol + Alkane) Systems
rho1	698.68	kg/m3	298.20	Isobaric Vapor Liquid Equilibrium of Binary Systems of Hexane or Octane with 1,2-Dimethylbenzene or 1,3-Dimethylbenzene at 101.3 kPa

rho	702.54	kg/m ³	293.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rho	698.49	kg/m ³	298.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rho	694.44	kg/m ³	303.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rho	690.37	kg/m ³	308.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rho	686.29	kg/m ³	313.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure

rhoI	682.19	kg/m3	318.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	678.08	kg/m3	323.15	Volumetric and Transport Properties of Binary Mixtures of n-Octane + Ethanol, + 1-Propanol, + 1-Butanol, and + 1-Pentanol from (293.15 to 323.15) K at Atmospheric Pressure
rhoI	702.86	kg/m3	293.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhoI	698.85	kg/m3	298.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rhoI	694.80	kg/m3	303.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K

rho1	690.73	kg/m3	308.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rho1	686.63	kg/m3	313.15	Excess Molar Volumes and Viscosities of Binary Systems of Butylcyclohexane with n-Alkanes (C7 to C14) at T = 293.15 K to 313.15 K
rho1	698.64	kg/m3	298.15	Thermodynamics of Mixtures Containing a Strongly Polar Compound. 9. Liquid-Liquid Equilibria for epsilon-Caprolactam + Selected Alkanes
rho1	702.55	kg/m3	293.15	Density and Surface Tension of Binary Mixtures of 2,2,4-Trimethylpentane + n-Heptane, 2,2,4-Trimethylpentane + n-Octane, Ethyl Acetate + Benzene, and Butanenitrile + Benzene from (293.15 to 323.15) K
rho1	690.50	kg/m3	308.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene

rho1	698.60	kg/m3	298.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene
rho1	698.84	kg/m3	298.15	Liquid-liquid equilibria for (2-hydroxy benzaldehyde + n-alkane) mixtures. Intermolecular and proximity effects in systems containing hydroxyl and aldehyde groups
rho1	702.93	kg/m3	293.15	Surface tension and density of mixtures of m-xylene + n-alkane at 293.15 K: Analysis under the extended Langmuir and Shereshefsky models
rho1	698.40	kg/m3	298.15	Fully automatized apparatus for determining speed of sound for liquids in the temperature and pressure interval (283.15-343.15) K and (0.1-95) MPa
rho1	694.88	kg/m3	303.15	Thermodynamic behavior of thiophene with octane, 1-hexyl-3-methylimidazolium bromide, or 1-octyl-3-methylimidazolium bromide in dilute region at T = (288.15 to 303.15) K

rhoI	698.92	kg/m3	298.15	Thermodynamic behavior of thiophene with octane, 1-hexyl-3-methylimidazolium bromide, or 1-octyl-3-methylimidazolium bromide in dilute region at T = (288.15 to 303.15) K
rhoI	678.11	kg/m3	323.15	Densities and Viscosities of Corn Oil + n-Alkanes Blends from (288.15 to 343.15) K at 0.1 MPa
rhoI	703.00	kg/m3	293.15	Thermodynamic behavior of thiophene with octane, 1-hexyl-3-methylimidazolium bromide, or 1-octyl-3-methylimidazolium bromide in dilute region at T = (288.15 to 303.15) K
rhoI	706.99	kg/m3	288.15	Thermodynamic behavior of thiophene with octane, 1-hexyl-3-methylimidazolium bromide, or 1-octyl-3-methylimidazolium bromide in dilute region at T = (288.15 to 303.15) K
rhoI	698.86	kg/m3	298.15	Determination and correlation of (liquid + liquid) equilibria of ternary and quaternary systems with octane, decane, benzene and [BMpyr][DCA] at T = 298.15 K and atmospheric pressure
rhoI	698.60	kg/m3	298.15	(Liquid + liquid) equilibrium at T = 298.15 K for ternary mixtures of alkane + aromatic compounds + imidazolium-based ionic liquids

rho1	698.55	kg/m3	298.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures
rho1	694.50	kg/m3	303.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures
rho1	702.60	kg/m3	293.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures
rho1	710.61	kg/m3	283.15	Density, viscosity and excess molar volume of binary mixtures of tri-n-octylamine + diluents (n-heptane, n-octane, n-nonane, and n-decane) at various temperatures
rho1	698.60	kg/m3	298.15	Evaluation of ionic liquids as solvent for aromatic extraction: Experimental, correlation and COSMO-RS predictions

rho1	698.75	kg/m3	298.15	Thermodynamics of mixtures containing amines. XI. Liquid + liquid equilibria and molar excess enthalpies at 298.15 K for N-methylaniline + hydrocarbon systems. Characterization in terms of DISQUAC and ERAS models
rho1	698.73	kg/m3	298.15	Excess molar enthalpies of the ternary mixtures: (tetrahydrofuran or 2-methyltetrahydrofuran + methyl tert-butyl ether + n-octane) at the temperature 298.15 K
rho1	698.86	kg/m3	298.15	Application of the ionic liquid tributylmethylammonium bis(trifluoromethylsulfonyl)imide as solvent for the extraction of benzene from octane and decane at T = 298.15 K and atmospheric pressure
rho1	698.86	kg/m3	298.15	Study of the suitability of two ammonium-based ionic liquids for the extraction of benzene from its mixtures with aliphatic hydrocarbons.
rho1	686.39	kg/m3	313.15	Liquid liquid equilibria for the ternary system water + octane + 2-butyloxy-ethanol
rho1	702.64	kg/m3	293.15	Liquid liquid equilibria for the ternary system water + octane + 2-butyloxy-ethanol

rhoI	698.61	kg/m3	298.15	Isobaric vapor-liquid equilibrium data of the binary systems of octane with p, o, m-xylene at 20 kPa
rhoI	698.51	kg/m3	298.10	Excess enthalpies of binary mixtures of 2-ethoxyethanol with four hydrocarbons at 298.15, 308.15, and 318.15K An experimental and theoretical study
rhoI	698.50	kg/m3	298.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhoI	702.50	kg/m3	293.15	Densities and Kinematic Viscosities of a Quinary Regular Liquid System and Its Five Quaternary Subsystems at 293.15A K and 298.15A K
rhoI	698.50	kg/m3	298.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K
rhoI	702.50	kg/m3	293.15	Densities and Kinematic Viscosities of One Quinary Regular Liquid System and Its Five Quaternary Sub-Systems at Temperatures (293.15 and 298.15) K
rhoI	703.00	kg/m3	293.00	KDB

rhoI	698.64	kg/m ³	298.15	Thermodynamics of mixtures containing amines VI. Liquid liquid equilibria for mixtures of o-toluidine + selected alkanes
rhoI	714.31	kg/m ³	278.15	Experimental Liquid Densities of n-Pentane, n-Octane, and n-Nonane and Their Binary Mixtures from (273.15 to 363.15) K at 0.1 MPa
rhoI	682.20	kg/m ³	318.15	The density, the refractive index and the adjustment of the excess thermodynamic properties by means of the multiple linear regression method for the ternary system ethylbenzene-octane-propylbenzene
sfust	93.19	J/molxK	215.60	NIST Webbook
sfust	95.70	J/molxK	215.80	NIST Webbook
sfust	95.85	J/molxK	216.38	NIST Webbook
speedsl	1130.30	m/s	308.15	Excess Enthalpy, Density, and Speed of Sound for the Ternary Mixture Methyl tert-Butyl Ether (1) + Butan-1-ol (2) + Octane (3)
speedsl	1151.00	m/s	303.15	Excess Enthalpy, Density, and Speed of Sound for the Ternary Mixture Methyl tert-Butyl Ether (1) + Butan-1-ol (2) + Octane (3)
speedsl	1171.90	m/s	298.15	Excess Enthalpy, Density, and Speed of Sound for the Ternary Mixture Methyl tert-Butyl Ether (1) + Butan-1-ol (2) + Octane (3)

speedsl	1193.00	m/s	293.15	Excess Enthalpy, Density, and Speed of Sound for the Ternary Mixture Methyl tert-Butyl Ether (1) + Butan-1-ol (2) + Octane (3)
speedsl	1213.60	m/s	288.15	Excess Enthalpy, Density, and Speed of Sound for the Ternary Mixture Methyl tert-Butyl Ether (1) + Butan-1-ol (2) + Octane (3)
srf	0.02	N/m	298.15	Interfacial tensions of binary mixtures of ethanol with octane, decane, dodecane, and tetradecane
srf	0.02	N/m	308.15	Interfacial tensions of binary mixtures of ethanol with octane, decane, dodecane, and tetradecane
srf	0.02	N/m	318.15	Interfacial tensions of binary mixtures of ethanol with octane, decane, dodecane, and tetradecane
srf	0.02	N/m	308.15	Surface Tension of Dialkyl Carbonates + (Alkanes or 1,4-Dimethylbenzene) and 1,4-Dimethylbenzene + Alkanes Binary Mixtures at T = 308.15 K
srf	0.02	N/m	293.20	KDB
srf	0.02	N/m	298.15	Analysis of Surface Tension, Density, and Speed of Sound for the Ternary Mixture Dimethyl Carbonate + p-Xylene + n-Octane

tcondl	0.12	W/m×K	334.80	Thermal Conductivities of [bmim][PF6], [hmim][PF6], and [omim][PF6] from 294 to 335 K at Pressures up to 20 MPa.
tcondl	0.12	W/m×K	314.70	Thermal Conductivities of [bmim][PF6], [hmim][PF6], and [omim][PF6] from 294 to 335 K at Pressures up to 20 MPa.
tcondl	0.13	W/m×K	294.50	Thermal Conductivities of [bmim][PF6], [hmim][PF6], and [omim][PF6] from 294 to 335 K at Pressures up to 20 MPa.

Pressure Dependent Properties

Property code	Value	Unit	Pressure [kPa]	Source
tbp	352.83	K	22.95	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	360.22	K	29.98	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	366.89	K	37.87	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

tbp	371.89	K	44.82	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	376.93	K	52.81	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	380.87	K	59.85	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	384.36	K	66.66	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	388.38	K	75.23	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	391.59	K	82.72	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
tbp	394.32	K	89.51	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures

tbp	397.87	K	99.01	A novel dynamic recirculating apparatus for vapour-liquid equilibrium measurements at moderate pressures and temperatures
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Correlations

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/(T + C)$
Coeff. A	1.44378e+01
Coeff. B	-3.45148e+03
Coeff. C	-4.72760e+01
Temperature range (K), min.	291.19
Temperature range (K), max.	425.47

Information	Value
Property code	pvap
Equation	$\ln(P_{vp}) = A + B/T + C \cdot \ln(T) + D \cdot T^2$
Coeff. A	6.57782e+01
Coeff. B	-6.98194e+03
Coeff. C	-7.37874e+00
Coeff. D	3.38092e-06
Temperature range (K), min.	216.38
Temperature range (K), max.	568.83

Datasets

Thermal conductivity, W/m/K

Temperature, K - Liquid	Pressure, kPa - Liquid	Thermal conductivity, W/m/K - Liquid
255.43	100.00	0.1386

255.34	5200.00	0.1409
255.48	10100.00	0.1427
255.80	20000.00	0.1458
255.12	30000.00	0.1482
274.91	100.00	0.1318
275.13	5000.00	0.1338
275.12	10200.00	0.1358
274.99	20200.00	0.1400
275.01	30200.00	0.1438
295.39	200.00	0.1265
295.22	5100.00	0.1287
295.33	10200.00	0.1309
295.18	20000.00	0.1351
295.13	30000.00	0.1391
315.13	100.00	0.1201
315.18	5000.00	0.1227
315.06	10000.00	0.1252
315.14	20200.00	0.1299
315.00	30000.00	0.1340
334.94	100.00	0.1143
334.97	5100.00	0.1170
335.05	10000.00	0.1194
334.94	20100.00	0.1245
334.94	30000.00	0.1288
355.08	100.00	0.1084
354.92	5000.00	0.1114
355.03	10000.00	0.1142
355.02	20000.00	0.1194
354.99	30000.00	0.1242
375.06	400.00	0.1019
374.87	5100.00	0.1052
375.08	10200.00	0.1082
374.90	20000.00	0.1147
375.26	30000.00	0.1198

Reference

<https://www.doi.org/10.1021/acs.jced.9b00628>

Molar heat capacity at constant pressure, J/K/mol

Temperature, K - Liquid	Pressure, kPa - Liquid	Molar heat capacity at constant pressure, J/K/mol - Liquid
323.15	100.00	263.30

328.15	100.00	265.70
333.15	100.00	267.98
338.15	100.00	270.38
343.15	100.00	272.66
348.15	100.00	275.18
353.15	100.00	277.58
358.15	100.00	280.09
363.15	100.00	282.60
368.15	100.00	285.11
373.15	100.00	287.86
378.15	100.00	290.37
383.15	100.00	293.45
323.15	10130.00	260.90
328.15	10130.00	263.18
333.15	10130.00	265.58
338.15	10130.00	267.75
343.15	10130.00	270.04
348.15	10130.00	272.32
353.15	10130.00	274.49
358.15	10130.00	277.00
363.15	10130.00	279.17
368.15	10130.00	281.57
373.15	10130.00	283.97
378.15	10130.00	286.49
383.15	10130.00	288.88
388.15	10130.00	290.94
393.15	10130.00	292.88
398.15	10130.00	295.97

Reference

<https://www.doi.org/10.1016/j.jct.2017.03.034>

Viscosity, Pa*s

Temperature, K - Liquid	Pressure, kPa - Liquid	Viscosity, Pa*s - Liquid
273.15	100.00	0.0007050
273.15	10000.00	0.0007930
273.15	20000.00	0.0008710
273.15	30000.00	0.0009710
293.15	100.00	0.0005440
293.15	10000.00	0.0005960
293.15	20000.00	0.0006590

293.15	30000.00	0.0007170
313.15	100.00	0.0004290
313.15	10000.00	0.0004830
313.15	20000.00	0.0005360
313.15	30000.00	0.0005930
333.15	100.00	0.0003510
333.15	10000.00	0.0003880
333.15	20000.00	0.0004410
333.15	30000.00	0.0004820

Reference

<https://www.doi.org/10.1007/s10765-006-0053-2>

Temperature, K

Pressure, kPa

Viscosity, Pa*s

303.15	101.33	0.0004918
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Reference

<https://www.doi.org/10.1016/j.fluid.2010.10.009>

Temperature, K

Pressure, kPa

Viscosity, Pa*s

298.24	100.00	0.0005080
308.72	5000.00	0.0004786
308.72	10000.00	0.0005043
323.93	100.00	0.0003829
348.64	100.00	0.0003034
349.46	5000.00	0.0003187
349.46	10000.00	0.0003364
394.81	5000.00	0.0002197
394.81	10000.00	0.0002334
436.86	5000.00	0.0001672
436.86	10000.00	0.0001799
467.46	5000.00	0.0001338
467.46	10000.00	0.0001458

Reference

<https://www.doi.org/10.1016/j.jct.2006.01.012>

Temperature, K

Pressure, kPa

Viscosity, Pa*s

323.15	100.00	0.0003892
323.15	10096.00	0.0004400
323.15	20701.00	0.0004950
323.15	30654.00	0.0005300
323.15	41050.00	0.0005760
323.15	54543.00	0.0006330

323.15	68036.00	0.0006930
348.14	100.00	0.0003011
348.14	7551.00	0.0003338
348.14	13680.00	0.0003513
348.14	20500.00	0.0003780
348.14	27466.00	0.0004008
348.14	27469.00	0.0004000
348.14	34305.00	0.0004240
348.14	34314.00	0.0004240
348.14	41226.00	0.0004490
348.14	41227.00	0.0004490
348.14	48070.00	0.0004710
348.14	55000.00	0.0004980
348.14	55004.00	0.0004990
348.14	61992.00	0.0005220
348.14	61994.00	0.0005330
373.12	6723.00	0.0002757
373.12	6724.00	0.0002758
373.12	20592.00	0.0003205
373.12	20599.00	0.0003217
373.12	27397.00	0.0003429
373.12	27402.00	0.0003429
373.12	34317.00	0.0003646
373.12	34324.00	0.0003649
373.12	41184.00	0.0003810
373.12	41207.00	0.0003800
373.12	41221.00	0.0003840
373.12	48024.00	0.0004090
373.12	48032.00	0.0004090
373.12	54853.00	0.0004330
373.12	54866.00	0.0004320
373.12	61686.00	0.0004470
373.12	61704.00	0.0004490
423.09	14725.00	0.0002290
423.09	27159.00	0.0002520
423.09	40831.00	0.0002870
423.09	54591.00	0.0003440
423.09	68420.00	0.0003520

Reference

<https://www.doi.org/10.1021/je0503296>

Temperature, K

Pressure, kPa

Viscosity, Pa*s

298.15	100.00	0.0005100
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298.15	20900.00	0.0006310
298.15	40600.00	0.0007530
298.15	60900.00	0.0008890
298.15	80000.00	0.0010400
298.15	80100.00	0.0010300
298.15	100300.00	0.0011900
298.15	120100.00	0.0013600
298.15	139700.00	0.0015550
298.15	139900.00	0.0015500
298.15	159500.00	0.0017500
298.15	179600.00	0.0019800
298.15	197200.00	0.0022100
323.15	100.00	0.0003870
323.15	20100.00	0.0004770
323.15	40000.00	0.0005700
323.15	60600.00	0.0006720
323.15	80100.00	0.0007780
323.15	101000.00	0.0008970
323.15	120300.00	0.0010100
323.15	141500.00	0.0011500
323.15	141600.00	0.0011500
323.15	160300.00	0.0012800
323.15	180700.00	0.0014400
323.15	201800.00	0.0016100
323.15	100.00	0.0003870
323.15	80100.00	0.0007810
348.15	100.00	0.0003040
348.15	20400.00	0.0003810
348.15	40800.00	0.0004570
348.15	60700.00	0.0005340
348.15	80100.00	0.0006140
348.15	101000.00	0.0007060
348.15	120400.00	0.0007940
348.15	140200.00	0.0008930
348.15	140300.00	0.0008920
348.15	160700.00	0.0009970
348.15	180800.00	0.0011100
348.15	201900.00	0.0012300
348.15	100.00	0.0003040
348.15	80100.00	0.0006140
373.15	100.00	0.0002450
373.15	20600.00	0.0003120
373.15	39900.00	0.0003730
373.15	60000.00	0.0004370

373.15	80200.00	0.0005030
373.15	101100.00	0.0005760
373.15	120000.00	0.0006450
373.15	140900.00	0.0007260
373.15	160300.00	0.0008040
373.15	180500.00	0.0008900
373.15	200900.00	0.0009810
398.15	21600.00	0.0002630
398.15	42000.00	0.0003200
398.15	79400.00	0.0004260
398.15	80900.00	0.0004300
398.15	120900.00	0.0005500
398.15	159500.00	0.0006740
398.15	160200.00	0.0006760
398.15	192300.00	0.0007860
398.15	21600.00	0.0002650
423.15	21400.00	0.0002260
423.15	41100.00	0.0002760
423.15	80400.00	0.0003720
423.15	80700.00	0.0003720
423.15	121500.00	0.0004760
423.15	159700.00	0.0005810
423.15	161300.00	0.0005870
423.15	192500.00	0.0006760
423.15	21400.00	0.0002260
448.15	21000.00	0.0001920
448.15	41200.00	0.0002390
448.15	80500.00	0.0003240
448.15	81400.00	0.0003260
448.15	121500.00	0.0004140
448.15	159400.00	0.0005040
448.15	160300.00	0.0005040
448.15	193000.00	0.0005850
448.15	21000.00	0.0001920
473.15	19300.00	0.0001630
473.15	20000.00	0.0001640
473.15	41100.00	0.0002100
473.15	81100.00	0.0002890
473.15	81500.00	0.0002890
473.15	121100.00	0.0003670
473.15	160700.00	0.0004480
473.15	161300.00	0.0004490
473.15	193400.00	0.0005160

Mass density, kg/m³

Temperature, K - Liquid	Pressure, kPa - Liquid	Mass density, kg/m ³ - Liquid
288.15	100.00	706.6
288.15	5000.00	710.9
288.15	10000.00	714.7
288.15	20000.00	721.7
288.15	30000.00	728.1
288.15	40000.00	734.3
298.15	100.00	698.6
298.15	5000.00	703.4
298.15	10000.00	707.0
298.15	20000.00	714.6
298.15	30000.00	721.4
298.15	40000.00	727.7
308.15	100.00	690.5
308.15	5000.00	695.0
308.15	10000.00	699.4
308.15	20000.00	707.3
308.15	30000.00	714.5
308.15	40000.00	720.8

Reference

<https://www.doi.org/10.1016/j.jct.2012.11.011>

Temperature, K	Pressure, kPa	Mass density, kg/m ³
293.15	101.00	702.58
303.15	101.00	694.48
313.15	101.00	686.32
323.15	101.00	678.09
288.15	100.00	706.5
288.15	1000.00	707.2
288.15	5000.00	710.3
288.15	10000.00	714.1
288.15	15000.00	717.7
288.15	20000.00	721.2
288.15	25000.00	724.5
288.15	30000.00	727.7

288.15	35000.00	730.8
288.15	40000.00	733.7
288.15	45000.00	736.5
288.15	50000.00	739.2
288.15	55000.00	741.7
288.15	60000.00	744.1
293.15	100.00	702.5
293.15	1000.00	703.2
293.15	5000.00	706.4
293.15	10000.00	710.3
293.15	15000.00	714.0
293.15	20000.00	717.6
293.15	25000.00	721.0
293.15	30000.00	724.3
293.15	35000.00	727.5
293.15	40000.00	730.5
293.15	45000.00	733.3
293.15	50000.00	736.0
293.15	55000.00	738.6
293.15	60000.00	741.0
298.15	100.00	698.5
298.15	1000.00	699.2
298.15	5000.00	702.5
298.15	10000.00	706.5
298.15	15000.00	710.3
298.15	20000.00	714.0
298.15	25000.00	717.6
298.15	30000.00	720.9
298.15	35000.00	724.1
298.15	40000.00	727.2
298.15	45000.00	730.1
298.15	50000.00	732.9
298.15	55000.00	735.5
298.15	60000.00	738.0
303.15	100.00	694.4
303.15	1000.00	695.2
303.15	5000.00	698.6
303.15	10000.00	702.7
303.15	15000.00	706.7
303.15	20000.00	710.5
303.15	25000.00	714.1
303.15	30000.00	717.5
303.15	35000.00	720.9
303.15	40000.00	724.0

303.15	45000.00	727.0
303.15	50000.00	729.8
303.15	55000.00	732.5
303.15	60000.00	735.0
308.15	100.00	690.4
308.15	1000.00	691.2
308.15	5000.00	694.7
308.15	10000.00	698.9
308.15	15000.00	703.0
308.15	20000.00	706.9
308.15	25000.00	710.6
308.15	30000.00	714.2
308.15	35000.00	717.5
308.15	40000.00	720.8
308.15	45000.00	723.8
308.15	50000.00	726.7
308.15	55000.00	729.4
308.15	60000.00	731.9
313.15	100.00	686.3
313.15	1000.00	687.1
313.15	5000.00	690.8
313.15	10000.00	695.1
313.15	15000.00	699.3
313.15	20000.00	703.3
313.15	25000.00	707.2
313.15	30000.00	710.8
313.15	35000.00	714.3
313.15	40000.00	717.6
313.15	45000.00	720.7
313.15	50000.00	723.6
313.15	55000.00	726.3
313.15	60000.00	728.9
318.15	100.00	682.2
318.15	1000.00	683.0
318.15	5000.00	686.8
318.15	10000.00	691.3
318.15	15000.00	695.6
318.15	20000.00	699.7
318.15	25000.00	703.6
318.15	30000.00	707.4
318.15	35000.00	711.0
318.15	40000.00	714.3
318.15	45000.00	717.5
318.15	50000.00	720.5

318.15	55000.00	723.3
318.15	60000.00	725.9
323.15	100.00	678.0
323.15	1000.00	678.9
323.15	5000.00	682.8
323.15	10000.00	687.4
323.15	15000.00	691.9
323.15	20000.00	696.1
323.15	25000.00	700.2
323.15	30000.00	704.0
323.15	35000.00	707.7
323.15	40000.00	711.1
323.15	45000.00	714.4
323.15	50000.00	717.4
323.15	55000.00	720.3
323.15	60000.00	722.9
328.15	100.00	673.8
328.15	1000.00	674.7
328.15	5000.00	678.7
328.15	10000.00	683.5
328.15	15000.00	688.1
328.15	20000.00	692.5
328.15	25000.00	696.7
328.15	30000.00	700.7
328.15	35000.00	704.4
328.15	40000.00	707.9
328.15	45000.00	711.3
328.15	50000.00	714.4
328.15	55000.00	717.3
328.15	60000.00	719.9
333.15	100.00	669.7
333.15	1000.00	670.6
333.15	5000.00	674.8
333.15	10000.00	679.7
333.15	15000.00	684.5
333.15	20000.00	689.0
333.15	25000.00	693.2
333.15	30000.00	697.3
333.15	35000.00	701.1
333.15	40000.00	704.7
333.15	45000.00	708.1
333.15	50000.00	711.3
333.15	55000.00	714.2
333.15	60000.00	716.9

343.15	100.00	661.2
343.15	1000.00	662.2
343.15	5000.00	666.6
343.15	10000.00	671.9
343.15	15000.00	677.0
343.15	20000.00	681.8
343.15	25000.00	686.3
343.15	30000.00	690.6
343.15	35000.00	694.6
343.15	40000.00	698.4
343.15	45000.00	701.9
343.15	50000.00	705.2
343.15	55000.00	708.2
343.15	60000.00	711.0
353.15	100.00	652.6
353.15	1000.00	653.7
353.15	5000.00	658.4
353.15	10000.00	664.1
353.15	15000.00	669.4
353.15	20000.00	674.5
353.15	25000.00	679.3
353.15	30000.00	683.9
353.15	35000.00	688.1
353.15	40000.00	692.1
353.15	45000.00	695.7
353.15	50000.00	699.1
353.15	55000.00	702.3
353.15	60000.00	705.1
363.15	100.00	643.8
363.15	1000.00	645.0
363.15	5000.00	650.1
363.15	10000.00	656.1
363.15	15000.00	661.9
363.15	20000.00	667.3
363.15	25000.00	672.4
363.15	30000.00	677.2
363.15	35000.00	681.6
363.15	40000.00	685.8
363.15	45000.00	689.6
363.15	50000.00	693.1
363.15	55000.00	696.3
363.15	60000.00	699.2
373.15	100.00	634.7
373.15	1000.00	636.3

373.15	5000.00	641.8
373.15	10000.00	648.2
373.15	15000.00	654.4
373.15	20000.00	660.1
373.15	25000.00	665.5
373.15	30000.00	670.6
373.15	35000.00	675.3
373.15	40000.00	679.6
373.15	45000.00	683.6
373.15	50000.00	687.3
373.15	55000.00	690.5
373.15	60000.00	693.5
393.15	100.00	616.3
393.15	1000.00	618.1
393.15	5000.00	624.3
393.15	10000.00	631.8
393.15	15000.00	638.8
393.15	20000.00	645.3
393.15	25000.00	651.5
393.15	30000.00	657.1
393.15	35000.00	662.3
393.15	40000.00	667.1
393.15	45000.00	671.4
393.15	50000.00	675.3
393.15	55000.00	678.8
393.15	60000.00	681.8
413.15	1000.00	599.3
413.15	5000.00	606.6
413.15	10000.00	615.1
413.15	15000.00	623.1
413.15	20000.00	630.6
413.15	25000.00	637.4
413.15	30000.00	643.8
413.15	35000.00	649.6
413.15	40000.00	654.8
413.15	45000.00	659.5
413.15	50000.00	663.6
413.15	55000.00	667.2
413.15	60000.00	670.2

Reference

<https://www.doi.org/10.1016/j.jct.2016.04.014>

Pressure, kPa

Temperature, K

Mass density, kg/m³

100.00

298.15

698.71

Reference

<https://www.doi.org/10.1016/j.jct.2017.09.027>**Temperature, K****Pressure, kPa****Mass density, kg/m³**

293.21

1996.00

703.76

293.22

3994.00

705.71

293.22

6001.00

707.57

293.21

8004.00

709.25

293.22

10009.00

710.88

293.21

13010.00

713.21

293.22

16009.00

715.43

293.22

19011.00

717.57

293.22

22012.00

719.76

293.22

25004.00

721.88

293.22

28004.00

724.19

293.21

30002.00

725.54

313.11

2007.00

688.27

313.11

4000.00

690.26

313.10

5999.00

692.07

313.11

7997.00

693.85

313.11

10009.00

695.59

313.11

13005.00

698.26

313.11

16009.00

700.84

313.10

19006.00

703.5

313.10

21998.00

706.05

313.10

25000.00

708.39

313.10

27998.00

710.67

313.10

30001.00

712.15

333.01

2005.00

672.19

333.01

3993.00

674.49

333.01

5998.00

676.69

333.01

8014.00

678.82

333.01

10007.00

680.8

333.01

13004.00

683.6

333.01

16002.00

686.47

333.01

19006.00

689.24

333.00

22003.00

691.91

333.01

25006.00

694.49

333.01

28003.00

696.99

333.01

30012.00

698.61

353.12

2008.00

655.38

353.12

3999.00

657.99

353.12	6000.00	660.5
353.12	8001.00	663.11
353.12	10006.00	665.45
353.13	13003.00	668.83
353.13	16004.00	672.05
353.12	19000.00	674.99
353.12	22003.00	677.96
353.12	25005.00	680.81
353.12	28008.00	683.56
353.12	30004.00	685.34

Reference

<https://www.doi.org/10.1021/acs.jced.7b00650>

Speed of sound, m/s

Temperature, K - Liquid	Pressure, kPa - Liquid	Speed of sound, m/s - Liquid
296.97	100.00	1173.0
303.61	100.00	1151.7
318.37	100.00	1089.5
332.50	100.00	1029.1
347.68	100.00	970.1
362.53	100.00	912.3
377.50	100.00	855.4
391.61	100.00	806.4
297.28	4000.00	1196.5
303.53	4000.00	1172.7
318.30	4000.00	1121.2
332.26	4000.00	1066.7
347.40	4000.00	1007.2
362.28	4000.00	955.4
377.03	4000.00	909.7
390.80	4000.00	860.1
407.38	4000.00	802.1
412.59	4000.00	786.2
422.73	4000.00	747.2
431.82	4000.00	720.1
442.23	4000.00	682.1
452.55	4000.00	646.4
462.37	4000.00	614.7
472.05	4000.00	579.7
482.98	4000.00	543.0

493.41	4000.00	503.5
502.54	4000.00	477.8
513.00	4000.00	439.1
522.92	4000.00	407.7
532.23	4000.00	373.2
537.40	4000.00	354.7
542.87	4000.00	337.8
546.68	4000.00	325.7
550.42	4000.00	315.2
557.27	4000.00	290.5
561.20	4000.00	276.7
567.01	4000.00	257.3
570.16	4000.00	245.6
297.34	7000.00	1222.0
303.33	7000.00	1199.7
318.35	7000.00	1141.4
332.33	7000.00	1089.1
347.29	7000.00	1031.9
362.17	7000.00	979.6
377.33	7000.00	933.5
391.00	7000.00	892.3
407.46	7000.00	836.9
412.65	7000.00	818.8
422.88	7000.00	784.5
431.88	7000.00	754.2
442.49	7000.00	723.8
452.64	7000.00	689.9
462.45	7000.00	660.1
472.15	7000.00	631.6
483.04	7000.00	599.7
493.48	7000.00	565.4
502.73	7000.00	537.1
513.26	7000.00	506.5
523.46	7000.00	478.6
532.36	7000.00	450.6
537.75	7000.00	436.8
543.83	7000.00	422.0
547.82	7000.00	406.8
552.01	7000.00	398.1
558.19	7000.00	380.2
561.87	7000.00	372.6
566.82	7000.00	356.5
570.20	7000.00	347.6
573.03	7000.00	341.0

575.57	7000.00	332.6
578.92	7000.00	323.1
297.38	10000.00	1242.7
303.38	10000.00	1213.7
318.11	10000.00	1164.8
332.32	10000.00	1108.6
347.37	10000.00	1053.4
362.12	10000.00	1006.2
377.35	10000.00	960.5
391.09	10000.00	917.4
407.45	10000.00	865.2
412.71	10000.00	846.7
422.61	10000.00	818.2
431.92	10000.00	789.8
442.65	10000.00	755.7
452.77	10000.00	728.1
465.54	10000.00	695.8
472.28	10000.00	676.9
483.12	10000.00	646.1
493.62	10000.00	614.7
502.95	10000.00	590.5
513.46	10000.00	563.1
523.60	10000.00	533.3
532.59	10000.00	511.4
538.10	10000.00	497.5
544.52	10000.00	483.1
548.60	10000.00	471.5
552.52	10000.00	465.1
558.64	10000.00	448.0
562.27	10000.00	441.3
566.96	10000.00	430.4
570.48	10000.00	424.0
573.37	10000.00	414.0
576.28	10000.00	408.7
579.36	10000.00	400.8
297.35	12000.00	1250.8
303.42	12000.00	1233.0
318.37	12000.00	1184.5
332.56	12000.00	1128.3
347.46	12000.00	1072.7
363.67	12000.00	1027.8
379.75	12000.00	973.9
394.67	12000.00	920.8
403.71	12000.00	896.1

414.33	12000.00	864.0
422.69	12000.00	844.3
431.77	12000.00	815.2
442.73	12000.00	779.7
452.88	12000.00	750.8
462.61	12000.00	724.2
472.38	12000.00	693.8
483.14	12000.00	672.7
493.73	12000.00	645.0
503.17	12000.00	616.5
513.67	12000.00	591.5
523.17	12000.00	570.6
532.79	12000.00	545.1
538.41	12000.00	530.4
543.27	12000.00	520.1
549.27	12000.00	505.4
552.88	12000.00	500.8
559.37	12000.00	486.2
562.71	12000.00	477.8
567.10	12000.00	471.0
570.75	12000.00	461.0
573.60	12000.00	454.4
576.53	12000.00	451.3
579.57	12000.00	444.1

Reference

<https://www.doi.org/10.1021/acs.jced.7b00712>

Sources

- Measurement of Critical Properties for Binary and Ternary Mixtures <https://www.doi.org/10.1021/acs.jced.8b00585>
- Measurements of activity coefficients at infinite dilution for organic solutes and water in the infinite dilution <https://www.doi.org/10.1016/j.jct.2013.07.004>
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- Using 1-ethyl-3-methylpyridinium bis(trifluoromethylsulfonyl)amide as Ionic Liquid for Activity Coefficients at Infinite Dilution of Organic Solutes in the Presence of Ionic Liquids <https://www.doi.org/10.1016/j.fluid.2006.03.002>
- Measurement of activity coefficients at infinite dilution of organic solutes in the presence of ionic liquids <https://www.doi.org/10.1016/j.jct.2013.10.026>
- Activity Coefficients at Infinite Dilution for Hydrocarbons, 2,2,2-Trifluoroethanol, and Ethanol in Ionic Liquids <https://www.doi.org/10.1021/je1005517>
- Determination of Activity Coefficients for Separation of Hydrocarbons Mixtures based on Gamma-Infinitesimal Measurements <https://www.doi.org/10.1016/j.jct.2018.07.024>
- Measurement of VLE and c1 data and activity coefficients at infinite dilution and physicochemical properties for ionic liquids and CO₂-SILCO₂ ionic liquid <https://www.doi.org/10.1016/j.jct.2005.04.010>
- 4-(2-methoxyethyl)-4-methylmorpholinium bis(trifluoromethylsulfonyl)-amide: <https://www.doi.org/10.1016/j.jct.2011.11.021>

Activity coefficients at infinite dilution of alkanes and alkenes in various solvents	https://www.doi.org/10.1016/j.fluid.2009.05.007
Viscosity Measurements of Endothermic Fluids at Temperatures from 303 K to 673 K and Pressures up to 5.0 MPa: Mixtures of Ethylbenzene + Nitrobenzene and Ethylbenzene + Butylbenzene	https://www.doi.org/10.1021/acs.jced.6b00391
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://www.doi.org/10.1021/je049572f
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://www.doi.org/10.1016/j.fluid.2010.10.013
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://www.doi.org/10.1021/je4001894
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://www.doi.org/10.1016/j.jct.2018.05.003
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://www.doi.org/10.1016/j.fluid.2012.12.025
Activity Coefficients at Infinite Dilution for Organic Solutes Dissolved in Three Aromatic liquids	https://en.wikipedia.org/wiki/Joback_method
Liquid-liquid equilibria for the ternary system water + octane +	https://www.doi.org/10.1016/j.fluid.2015.04.019
Solubility of Mercury in Liquid Hydrocarbons and Hydrocarbon Mixtures:	https://www.doi.org/10.1021/acs.jced.6b00173

Legend

af:	Acentric Factor
aiqt:	Autoignition Temperature
ap:	Aniline Point
chl:	Standard liquid enthalpy of combustion
cpg:	Ideal gas heat capacity
cpl:	Liquid phase heat capacity
dm:	Dipole Moment
dvisc:	Dynamic viscosity
fll:	Lower Flammability Limit
flu:	Upper Flammability Limit
fpo:	Flash Point (Open Cup Method)
gf:	Standard Gibbs free energy of formation
gyrad:	Radius of Gyration
hcg:	Heat of Combustion, Gross form
hcn:	Heat of Combustion, Net Form
hf:	Enthalpy of formation at standard conditions
hfl:	Liquid phase enthalpy of formation at standard conditions
hfus:	Enthalpy of fusion at standard conditions
hfust:	Enthalpy of fusion at a given temperature
hsubt:	Enthalpy of sublimation at a given temperature
hvap:	Enthalpy of vaporization at standard conditions
hvapt:	Enthalpy of vaporization at a given temperature
ie:	Ionization energy
log10ws:	Log10 of Water solubility in mol/l
logp:	Octanol/Water partition coefficient
mcvol:	McGowan's characteristic volume
nfpaf:	NFPA Fire Rating
pc:	Critical Pressure

pvap:	Vapor pressure
rfi:	Refractive Index
rho:	Liquid Density
sfust:	Entropy of fusion at a given temperature
sg:	Molar entropy at standard conditions
sl:	Liquid phase molar entropy at standard conditions
speedsl:	Speed of sound in fluid
srf:	Surface Tension
tb:	Normal Boiling Point Temperature
tbp:	Boiling point at given pressure
tc:	Critical Temperature
tcondl:	Liquid thermal conductivity
tf:	Normal melting (fusion) point
tt:	Triple Point Temperature
vc:	Critical Volume
zc:	Critical Compressibility
zra:	Rackett Parameter

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